# CERTIFICATES OF COMPETENCY IN THE MERCHANT NAVY MARINE ENGINEER OFFICER 

EXAMINATIONS ADMINISTERED BY THE SCOTTISH QUALIFICATIONS AUTHORITY

ON BEHALF OF THE
MARITIME AND COASTGUARD AGENCY

STCW 95 CHIEF ENGINEER REG. III/2 (UNLIMITED)

041-32 - APPLIED HEAT

MONDAY, 4 APRIL 2016

1315-1615 hrs

Examination paper inserts:
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Notes for the guidance of candidates:

1. Non-programmable calculators may be used.
2. All formulae used must be stated and the method of working and ALL intermediate steps must be made clear in the answer.

## Materials to be supplied by examination centres:

Candidates examination workbook
Graph paper
'Thermodynamic and Transport Properties of Fluids' by Mayhew \& Rogers ( $5^{\text {th }}$ edition)

## APPLIED HEAT

Attempt SIX questions only.
All questions carry equal marks.
Marks for each part question are shown in brackets.

1. A volume of $0.02 \mathrm{~m}^{3}$ of air at a pressure and temperature of 1.05 bar and $15^{\circ} \mathrm{C}$ respectively is heated at constant volume until the pressure is 4.2 bar . It is then cooled at constant pressure to the initial temperature.
(a) Sketch the processes on a Temperature-specific entropy diagram.
(b) Calculate EACH of the following:
(i) the net heat flow;
(ii) the net change in entropy.

Note: for air $R=0.287 \mathrm{~kJ} / \mathrm{kgK}$ and $\gamma=1.4$
2. A Morse test was carried out on a 4 cylinder, 4 stroke compression ignition engine and the following data was noted.

Engine speed $3000 \mathrm{rev} / \mathrm{min}$, Full load brake torque 255 Nm . Air fuel ratio by mass 30:1,

| Morse test result |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: |
| Cylinder cut out | 1 | 2 | 3 | 4 |
| Brake Power kW | 57.77 | 57.40 | 57.11 | 57.90 |


| Data Table |  |  |  |  |  |  |  |
| :--- | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | Flow <br> rate <br> Litres/ <br> min | specific <br> heat <br> capacity <br> $\mathrm{kJ} / \mathrm{kg}$, | inlet <br> temperature <br> ${ }^{\circ} \mathrm{C}$ | outlet <br> temperature <br> ${ }^{\circ} \mathrm{C}$ | Density <br> $\mathrm{kg} / \mathrm{m}^{3}$ | Calorific <br> values <br> $\mathrm{MJ} / \mathrm{kg}$ |  |
| cooling <br> water | 9.87 | 4.18 | 48 | 80 | 1000 |  |  |
| lubricating <br> oil | 46.21 | 2.1 | 40 | 48 | 850 |  |  |
| Air |  |  | 45 |  |  |  |  |
| Gas |  | 1.15 |  | 450 |  |  |  |
| Fuel | 0.344 |  |  |  | 720 | 43 |  |

(a) Calculate EACH of the following:
(i) the indicated power;
(ii) the brake specific fuel consumption;
(iii) the indicated thermal efficiency.
(b) Draw up an energy balance as a percentage of the total energy supplied.
3. A fuel of mass analysis $84 \%$ carbon and $16 \%$ hydrogen is completely burned in air.

The dry flue gas analysis shows they contain $81 \%$ nitrogen by volume.
(a) Determine, using molar volumes, the full combustion equation for 1 kg of fuel.
(b) Calculate EACH of the following:
(i) the air fuel ratio by mass;
(ii) the mass of water condensed per kg of fuel when the flue gas is at 1.01 bar and $20^{\circ} \mathrm{C}$.

Note: Relative atomic masses $H=1, C=12, N=14, O=16$
Air contains $21 \%$ oxygen by volume.
The Molar mass of air may be taken as $29 \mathrm{~kg} / \mathrm{kmol}$.
4. In a regenerative steam power plant, steam enters the turbine at a pressure and temperature of 30 bar and $450^{\circ} \mathrm{C}$ respectively.
It then expands isentropically to a dry saturated condition at which point some steam is bled off to a direct contact feed heater.
The feed water leaves the heater 4.5 K below the saturation temperature of the bled steam pressure.
The remainder of the steam expands isentropically to a condenser pressure of 0.035 bar.

There is no under cooling in the condenser and the feed pump work may be ignored.
(a) Sketch the cycle on a temperature- specific entropy diagram.
(b) Determine EACH of the following:
(i) the mass flow rate of bled steam per kg of steam flowing;
(ii) the specific work output;
(iii) the thermal efficiency of the cycle.
5. The first stage of an impulse turbine is velocity compounded with two rows of moving blades.

The steam leaves the nozzles with an absolute velocity of $800 \mathrm{~m} / \mathrm{s}$ at an angle of $17^{\circ}$ to the plane of rotation.

The mean blade diameter is 750 mm and the exit angle from the first row of moving blades, the fixed blades and the second row of moving blades are $22^{\circ}$, $28^{\circ}$ and $36^{\circ}$ respectively.

The blade velocity coefficient is 0.92 over each of the three rows of blades.
The mass flow rate of steam is 6 tonne/hour and the turbine shaft speed is $3500 \mathrm{rev} / \mathrm{min}$.

Determine EACH of the following:
(a) the fixed and moving blade inlet angles;
(b) the power developed;
(c) the axial thrust acting on the rotor.
6. In a vapour compression refrigeration cycle Ammonia is compressed between saturation temperatures of $-12^{\circ} \mathrm{C}$ and $+22^{\circ} \mathrm{C}$.
The refrigerant is dry saturated at entry to the compressor and leaves the condenser with 4 degrees of under-cooling.
The cooling load is 1.5 MW and the isentropic efficiency of the compressor is 82\%.
(a) Sketch the cycle on P-h and T-s diagrams.
(b) Determine EACH of the following:
(i) the co-efficient of performance;
(ii) the compressor power in kW ;
(iii) the Carnot co-efficient of performance between the same pressure limits.
7. An annular cooling water jacket surrounds a 75 mm mean diameter pipe carrying a hot gas, in a counter flow arrangement.
The hot gas enters the cooler at $350^{\circ} \mathrm{C}$ and leaves at $100^{\circ} \mathrm{C}$. The cooling water enters the cooler at $10^{\circ} \mathrm{C}$.
The flow rate of the gas is $200 \mathrm{~kg} /$ hour and that of the water is $1400 \mathrm{~kg} / \mathrm{hour}$. The wall thickness of the pipe may be ignored.

Calculate EACH of the following:
(a) the exit temperature of the water;
(b) the log mean temperature difference;
(c) the length of the cooler.

Note: for cooling water $\mathrm{c}=4.19 \mathrm{~kJ} / \mathrm{kgK}$
for the hot gas $\quad c_{p}=1.13 \mathrm{~kJ} / \mathrm{kgK}$
the inner surface heat transfer coefficient $=0.3 \mathrm{~kW} / \mathrm{m}^{2} \mathrm{~K}$
the outer surface heat transfer coefficient $=1.5 \mathrm{~kW} / \mathrm{m}^{2} \mathrm{~K}$
8. In a single acting two stage reciprocating air compressor, air is compressed from an inlet pressure and temperature of 0.9 bar and $20^{\circ} \mathrm{C}$ respectively to a delivery pressure of 12 bar.

The low pressure cylinder has a bore of 250 mm , stroke of 160 mm and the clearance volume is $2.5 \%$ of the swept volume.

The air enters the second stage at a pressure and temperature of 3 bar and $35^{\circ} \mathrm{C}$ respectively.

The compressor speed is $300 \mathrm{rev} / \mathrm{min}$.
The index of compression and expansion in both stages is 1.25 .
The mechanical efficiency is 0.85 .
(a) Sketch the process on a p-V diagram.
(b) Calculate EACH of the following:
(i) the free air delivered per hour at free air conditions of 1 bar and $15^{\circ} \mathrm{C}$;
(ii) the input power required to drive the compressor;
(iii) the heat removed in the inter-cooler.

Note: for air $R=0.287 \mathrm{~kJ} / \mathrm{kgK} \quad c_{p}=1.005 \mathrm{~kJ} / \mathrm{kgK}$
9. Steam enters a convergent-divergent nozzle with negligible velocity and expands into a space at 5 bar.

At inlet the pressure is 15 bar and temperature is $400^{\circ} \mathrm{C}$.
The process from the inlet to the throat is isentropic with an index of 1.37. The process from the throat to the exit has an isentropic efficiency of 0.9.

Calculate EACH of the following:
(a) the condition of the steam at the throat;
(b) the velocity of the steam at the throat;
(c) the throat area for a mass flow of $1 \mathrm{~kg} / \mathrm{s}$;
(d) the exit velocity.

